

## sewage pump station

The excavation depth of sewerage system must not exceed 5m to avoid:

- 1- The excess cost of excavation.
- 2- Difficult maintenance at deep depth.
- 3- Difficult installation in the presence of ground water.

### Purpose:

- 1- To rise the sewage from the level of last manhole to the level of the first tank in the wastewater treatment plant (deceleration tank).
- 2- If the excavation depth exceeds 5m – 7m (depends on the type of soil) sewage pump station is needed to rise the sewage to a manhole of level 1.2m)

### Types of sewage pump station:

Rectangular and circular depends on type of soil and the available area.

### Types of pumps:

- 1- Dry pump.
  - Horizontal pump.
  - Vertical pump.
- 2- Submerged pump.
- 3- Screw pump.

### The sewage pump station consists of:

Pumps, wet sump, pumps chamber, and rising main.

### 1- pumps:

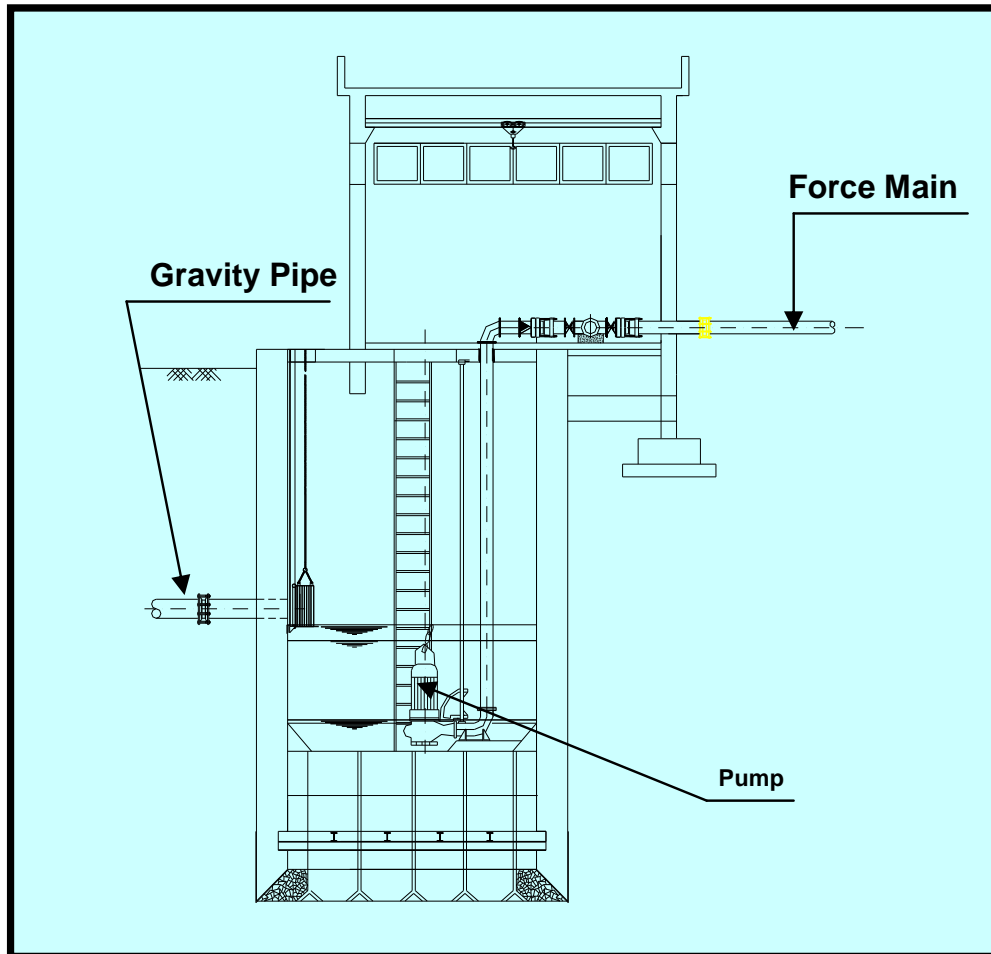
- The discharge of the pump doesn't exceed 300 l/s and the head of the pump doesn't exceed 90 m.
- The total number of pumps must not be less than 3 pumps (one pump is working and one pump is standing by and the other one is in maintenance ).

### Types of pumps

### Centrifugal pumps



## Submersible wastewater pumps



### **Total head of pump:**

HT=H static+h friction+h minor Losses +h Losses in P.S

Hstatic = H.W.L – L.W.L

= water level in the deceleration tank – L.W.L in the wet sump

Friction losses hf

$$h_f = \frac{4flv^2}{2gd}$$

Minor Losses = 10 % of hf

Losses in P.S = 2 – 5 m.

Qd = Qmax ( the bigger of Q max summer and Q max winter)

### **2- Wet sump:**

#### **Purpose:**

Collects and distributes the wastewater uniformly on the total number of pumps.

#### **Suction well**



#### **Suction pipes and the main header**



**Design criteria:**

- 1- T at Q max = 5 – 10 minutes  
T at Q min  $\leq$  30 minutes
- 2-  $v_s \leq 1.5$  m/s ( velocity in suction pipe)  
 $v_d \leq 2$  m/s ( velocity in delivery pipe)
- 3-  $d = 2$  m
- 4-  $B = 1 - 3$  m
- 5- The distance between pumps = 1.5 – 2.5 m
- 6-  $V = Qd \times T$

**3- Rising main:**

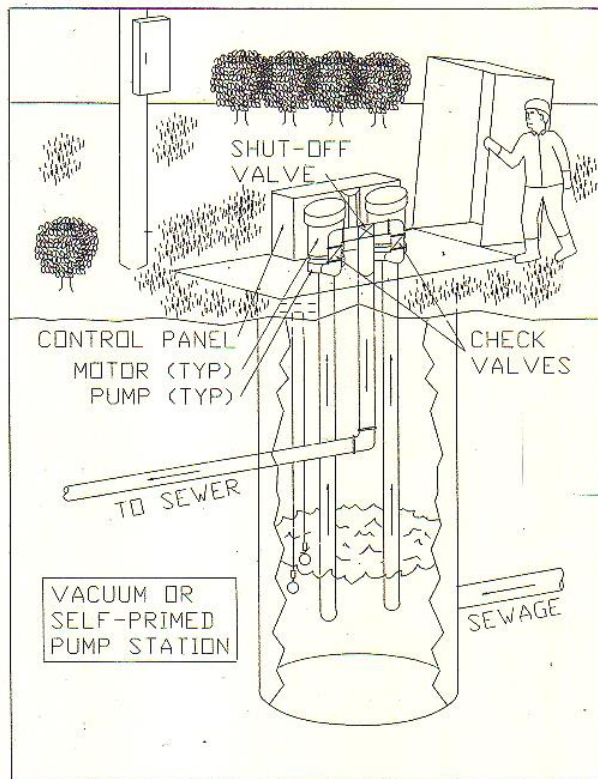
**Purpose:**

Transmit the wastewater from P.S to the deceleration tank.

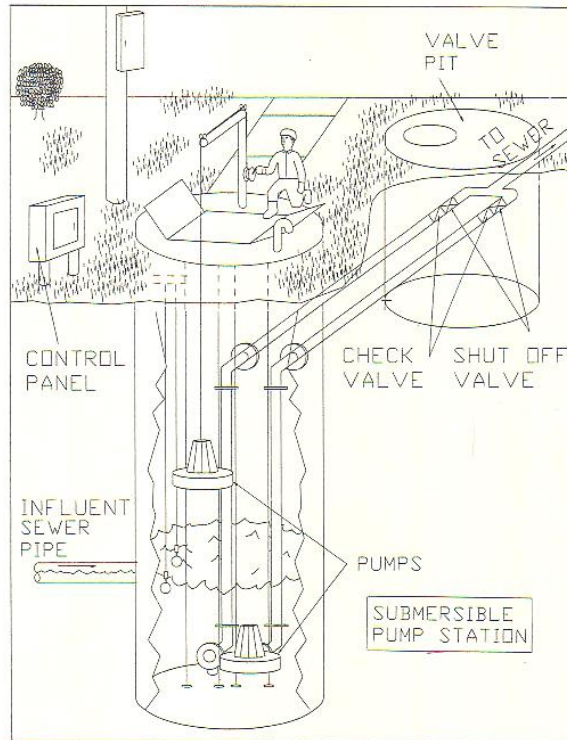
**Design criteria:**

- 1-  $Qd = A \times v$
- 2-  $v = 1 - 1.5$  m/s  $v \geq 1$  m/s
- 3- minimum  $\Phi = 100$  mm (ductile iron)
- 4-  $n \geq 2$

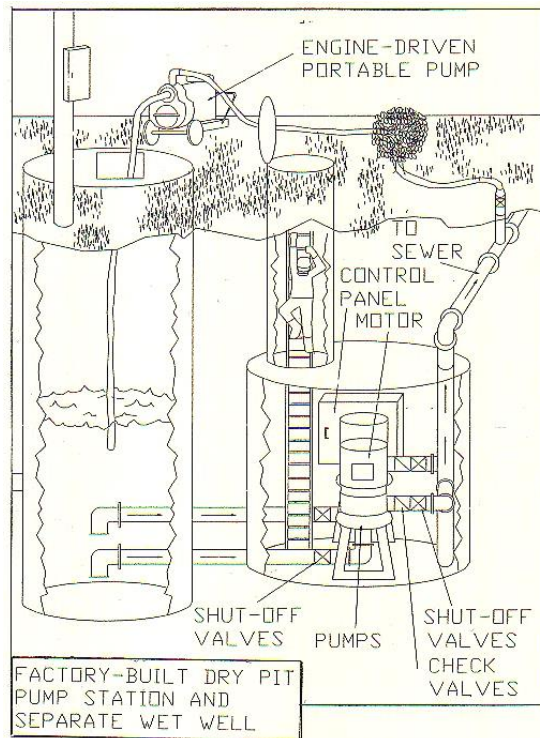
**Dry pump**



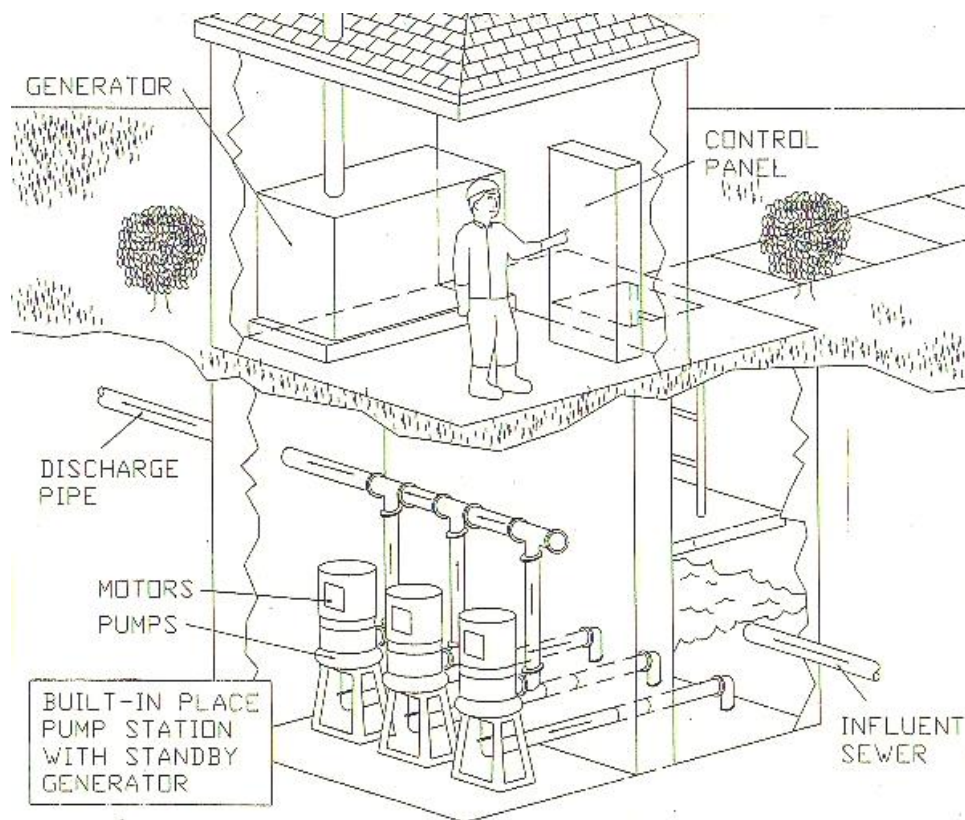
## Submerged pumps



## Dry pumps







**Example:**

For a city of present population 10.000 capita has average water consumption 180 l/c/d, and planned to be saturated at year 2050 with population 75.000 capita and average w.c. 280 l/c/d. it is required to design the following parts of its sewerage system as:

- Main collector of this district with invert level (-3.00) from the ground level.
- Pump station wet well & dry well type
- Force main with length 8.0 km up to WWTP where its ground level is (+12.00) & the water level in the first tank is above ground by 4.00m.

### For the main collector

$$Q_{ave} = 0.8 \times \frac{\text{pop} \times \text{w.c}}{24 \times 60 \times 60}$$
$$= 0.8 \times \frac{75000 \times 280}{24 \times 60 \times 60} = 194.44 \text{ l/s}$$

$$\text{P.F.F.} = 1 + \frac{14}{4 + \sqrt{\frac{\text{pop}}{1000}}}$$

$$\text{P.F.F.} = 1 + \frac{14}{4 + \sqrt{\frac{75000}{1000}}} = 2.11$$

$$\text{M.F.F.} = 0.2 \left( \frac{\text{pop}}{1000} \right)^{0.167}$$

$$\text{M.F.F.} = 0.2 \left( \frac{75000}{1000} \right)^{0.167} = 0.52$$

$$Q_{ave. \text{ Summer}} = 1.2 \times Q_{ave}$$
$$= 1.2 \times 194.44 = 233.33 \text{ l/s}$$

$$Q_{max \text{ summer}} = \text{P.F.F} \times Q_{ave \text{ summer}} + Q_{inf}$$
$$= 2.11 \times 233.33 + (10\% \times 194.44) = 511.77 \text{ l/s}$$

$$Q_{ave \text{ winter}} = 0.7 \times Q_{ave}$$
$$= 0.7 \times 194.44 = 136.11 \text{ l/s}$$

$$Q_{min \text{ winter}} = \text{M.F.F} \times Q_{min \text{ winter}} + Q_{inf}$$
$$= 0.52 \times 136.11 + 19.44 = 90.22 \text{ l/s}$$

Assume  $d / \emptyset = 0.75$  from chart (2)  $Q_{max.} / Q_{full.} = 0.86$

$$Q_{full.} = Q_{max.} / 0.86 = 511.77 / 0.86 = 595.08 \text{ l/s}$$

Assume  $V_{min.} = 0.6 \text{ m/s} \rightarrow$  self. Cleaning velocity

$$Q_{min.} / Q_{full.} = 90.22 / 595.08 = 0.15$$

from chart (2)  $V_{min.} / V_{full.} = 0.73$

$$V_{full.} = 0.6 / 0.73 = 0.82 \text{ m/s}$$

If we use PVC pipe  $n = 0.019$  &  $n$  of chart = 0.015

$$Q_{full. \text{ of chart}} \times n \text{ of chart} = Q_{full. \text{ act}} \times n \text{ act}$$

$$Q_{full. \text{ of chart}} = 595.08 \times 0.019 / 0.015 = 753.76 \text{ l/s}$$

$$V_{full. \text{ of chart}} = V_{full. \text{ act}} \times 0.019 / 0.015 = 1.04 \text{ m/s}$$

From chart (1) with  $Q_{full.}$  chart &  $V_{full.}$  chart

$\emptyset$ - 36" , S = 2.2 %

$Q_{\max} / Q_{\text{full act}} = 0.86$  & from chart  $V_{\max} / V_{\text{full}} = 1.07$

$V_{\max} = 1.07 \times 0.82 = 0.88 \text{ m/s}$  < 1.5 o.k.

## **ii. Pump station**

Design of Wet sump:

Q design  $\rightarrow$  Q max & Q min

Q max = 511.77 l/s  $\times$  60/1000 = 30.7 m<sup>3</sup>/min

Qmin = 90.22 l/s  $\times$  60/1000 = 5.41 m<sup>3</sup>/min

T = 5 - 10 minutes (at Qmax)

$V = Q_{\max} \times T$

$$= 30.7 \times 5 = 153.5 \text{ m}^3$$

d = 2 m

$A_{\text{wet}} = V/d$

$$= 153.5 / 2 = 76.75 \text{ m}^2$$

Take pump of wet & dry well type vertical centrifugal pump  
with Ratio 1/3 wet & 2/3 dry.

Total area of sump = 3  $\times$  76.75 = 230.25 m<sup>2</sup>

$A = \pi \Phi^2 / 4$

$$230.25 = \pi \Phi^2 / 4 \quad \therefore \Phi = 17.12 \text{ m}$$

Check at Qmin:

$V = Q_{\min} \times T$

$$T = 153.5 / 5.41 = 28.37 \text{ minutes} < 30 \text{ minutes} \text{ safe}$$

Design of force main

$Q = A \times v$

Take  $v = 1 \text{ m/s}$   $v = 1 - 1.5 \text{ m/s}$

$A = Q / v$

$$= 511.77 / 1000 / 1 = 0.51 \text{ m}^2$$

$A = \pi \Phi^2 / 4$

$$0.51 = \pi \Phi^2 / 4 \quad \therefore \Phi = 0.81 \sim 0.8 \text{ m}$$

$V_{\text{act}} = 1.02 \text{ m/s} < 2 \text{ o.k.}$



Pump head

$HT = H_{\text{static}} + H_{\text{friction}} + H_{\text{minor Losses}} + H_{\text{Losses in P.S}}$

Static head ( $H_s$ ) =  $12.00 + 4 + 3 + 0.5 + 1.75 = 21.25\text{m}$

Dynamic head = friction head loss + secondary loss

$$h_f = \frac{4fv^2}{2gd}$$

$$h_f = \frac{4 \times 0.008 \times 8000 \times 1.02^2}{2 \times 9.82 \times 0.8} = 16.95\text{m}$$

Total head =  $21.25 + 16.95 + 1.695 + 5 = 44.9\text{ m}$