

Primary Sedimentation tank

Purpose:

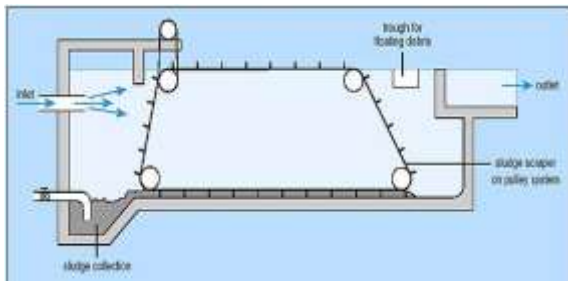
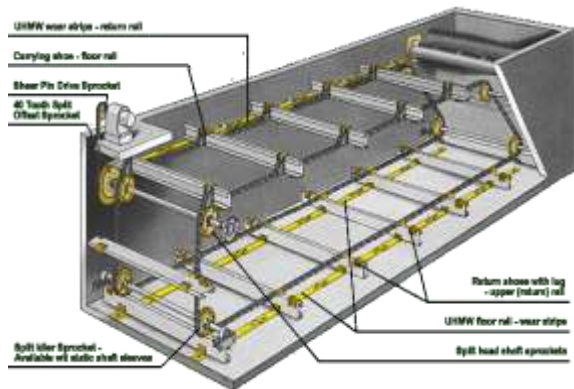
- 1- Removal of 40 - 60 % of suspended solids
- 2- Removal of 25 - 35 % of B.O.D.
- 3- Sediment the organic and inorganic matters to improve the properties of the sewage and prepare it for the biological treatment.

Types of primary sedimentation tanks:

- 1- Rectangular tank.
- 2- Circular tank.

Factors affecting sedimentation efficiency:

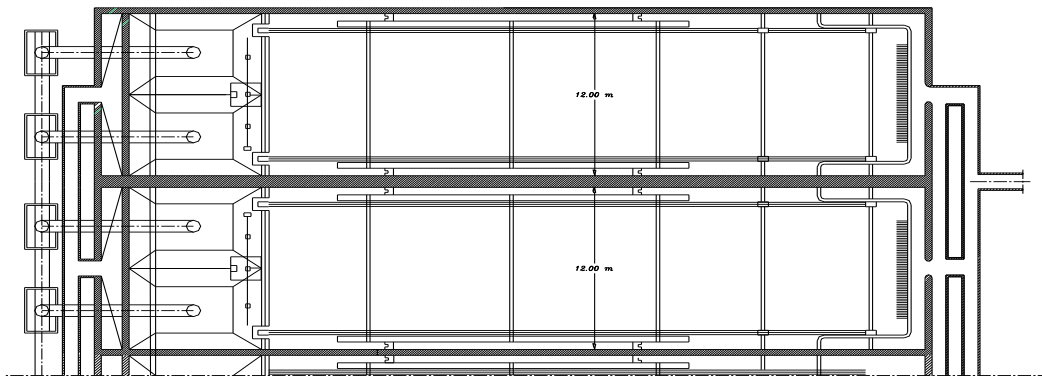
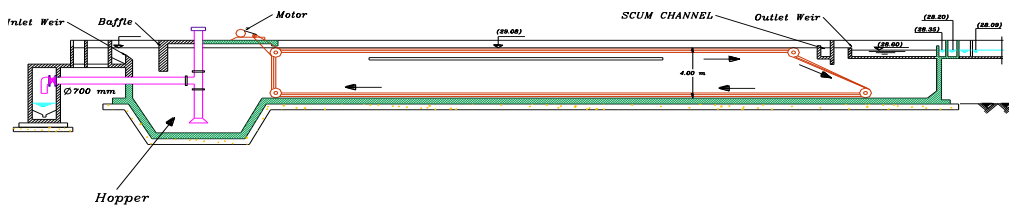
- 1- Viscosity
- 2- Concentration of suspended solids
- 3- Retention period
- 4- Horizontal velocity
- 5- Temperature
- 6- Surface loading rate = $24 - 48 \text{ m}^3/\text{m}^2/\text{day}$



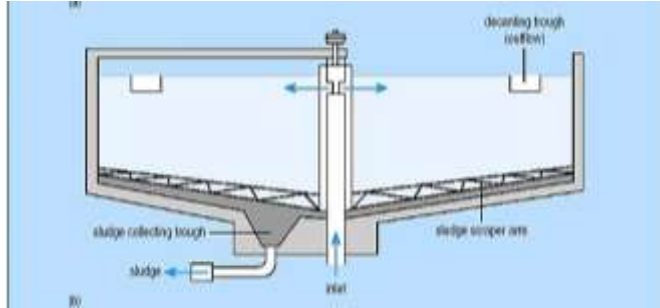
Primary sedimentation tank
(horizontal flow)



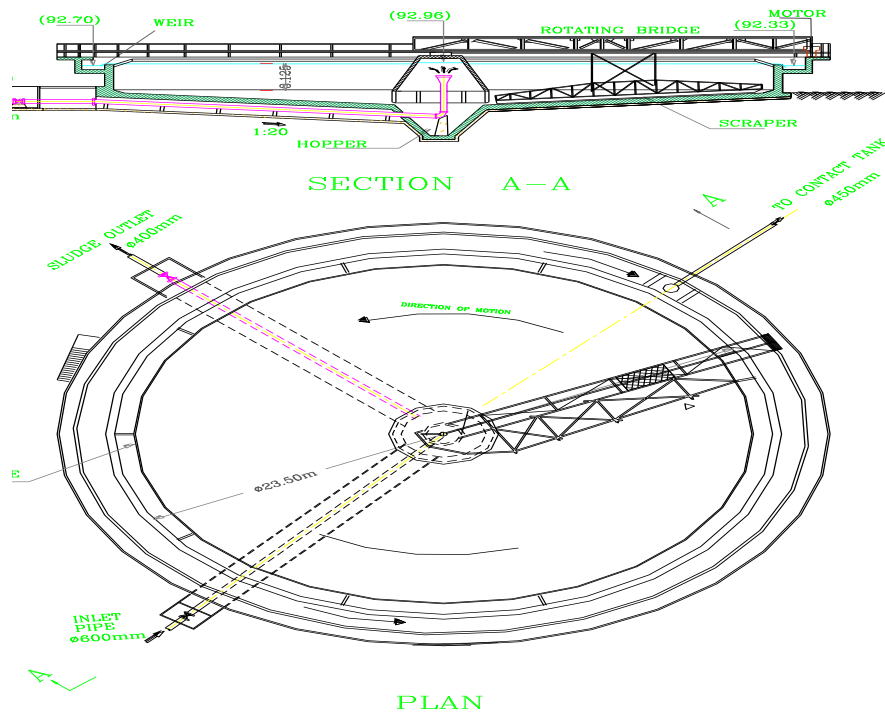
Effluent weir of rectangular sedimentation tank



Rectangular primary sedimentation tank



Primary sedimentation tank
(Radial flow)



Circular primary sedimentation tank

7- Dimension of tank

8- Dead zones.

Design criteria:

1- Retention period = $T = 2 - 3$ hrs

2- Surface loading rate (S.L.R.) = $24 - 48 \text{ m}^3/\text{m}^2/\text{day}$

3- Horizontal velocity $\leq 0.3 \text{ m/min}$

4- Effluent weir loading (E.W.L.) $\leq 600 \text{ m}^3/\text{m}/\text{day}$ ($\leq 25 \text{ m}^3/\text{m}/\text{hr}$)

5- $L = 3 - 5 B$

$$L \leq 40 \text{ m}$$

6- $d = 3 - 5 \text{ m}$

7- $B = 2 - 3 d$

8- $\Phi \leq 40 \text{ m}$

9- Bottom slope for circular tank = $4 - 10 \%$

for rectangular tank = $1 - 2 \%$

$$V = Q_d \times T$$

$$\text{S.L.R} = Q_d / \text{S.A}$$

Example:

For a sewage treatment plant, the following data are given:

- $Q_{\text{ave summer}} = 18000 \text{ m}^3/\text{d}$

- $\text{S.L.R} = 30 \text{ m}^3/\text{m}^2/\text{d}$

It is required to design primary sedimentation tanks.

Solution:

$$Q_d = 1.5 \times 18000 = 27000 \text{ m}^3/\text{d}$$

For rectangular tank:

Assume $T = 2.5 \text{ hr}$

$$V = Q_d \times T$$

$$= 27000 \times \frac{2.5}{24} = 2812.5 \text{ m}^3$$

$$\text{S.L.R} = \frac{Q_d}{\text{S.A}}$$

$$\text{S.A} = \frac{27000}{30} = 900 \text{ m}^2$$

$$d = \frac{V}{S.A}$$

$$= \frac{2812.5}{900} = 3.1 \text{ m}$$

Take $n = 2$

$$\therefore S.A \text{ of one tank} = \frac{900}{2} = 450 \text{ m}^2$$

Assume length = 40 m

$$b = \frac{S.A}{L} = \frac{450}{40} = 11.25 \text{ m}$$

Check:

$$1 - V_h = \frac{Q_d}{\text{cross sectional area}} = \frac{Q_d}{n \times b \times d}$$

$$= \frac{27000}{(2 \times 11.25 \times 3.1) \times 24 \times 60} = 0.269 < 0.3 \text{ m/min safe}$$

$$2 - E.W.L = \frac{Q_d}{n \times b}$$

$$= \frac{27000}{2 \times 11.25} = 1200 \text{ m}^3 / \text{m/d} > 600 \text{ unsafe}$$

\therefore take weir loading = $600 \text{ m}^3 / \text{m/d}$

$$\text{Length of weir} = \frac{Q_d}{\text{weir loading}} = \frac{27000}{2 \times 600} = 22.5 \text{ m}$$



Circular primary sedimentation tank:

$$V = Q_d \times T$$
$$= 27000 \times \frac{2.5}{24} = 2812.5 \text{ m}^3$$

$$S.L.R = \frac{Q_d}{S.A}$$

$$S.A = \frac{2700}{30} = 900 \text{ m}^2$$

$$d = \frac{V}{S.A}$$
$$= \frac{2700}{900} = 3.1 \text{ m}$$

Take $n = 2$

$$\therefore S.A \text{ of one tank} = \frac{900}{2} = 450 \text{ m}^2$$
$$= \frac{\pi \phi^2}{4}$$

$$\therefore \phi = 24 \text{ m}$$

Check :

$$1 - v_h = \frac{Q_d}{n \times \pi \times \phi \times d}$$
$$= \frac{27000}{2 \times \pi \times 24 \times 3.1 \times (24 \times 60)} = 0.04 \text{ m/min} < 0.3 \text{ m/min safe}$$

$$2 - E.W.L = \frac{Q_d}{n \times \pi \times \phi}$$
$$= \frac{27000}{n \times \pi \times 24} = 179 \text{ m}^3 / \text{m/d} < 600 \text{ safe}$$

Example:

Estimate the volume of sludge produced per 27000 m³/d if the influent S.S 300 mg/l. The removal efficiency is 60%.

Solution:

$$\text{Weight of dry solids} = \frac{60}{100} \times 300 \times 27000 \times 10^{-6} = 4.86 \text{ t/d}$$

$$\text{Specific gravity of sludge} = 1.03 \text{ t/m}^3$$

$$\text{Volume of dry solids} = \frac{\text{weight}}{\text{S.G}} = \frac{4.86}{1.03} = 4.718 \text{ m}^3 / \text{d}$$

$$\text{Moisture content of sludge} = 95\% \text{ (5\% solids)}$$

$$\text{Volume of sludge} = \frac{4.718}{0.05} = 94.37 \text{ m}^3 / \text{d}$$

Design of hopper:

$$\text{Volume of sludge per tank} = \frac{94.37}{2} = 47.18 \text{ m}^3 / \text{d}$$

$$\text{Volume of sludge per hopper} = \frac{47.18}{2} = 23.59 \text{ m}^3 / \text{d}$$

Assuming sludge withdrawal every 12 hours

$$\text{Volume of sludge per hopper} = \frac{23.59}{2} = 11.796 \text{ m}^3 / \text{d}$$

$$V = \frac{h}{3} (a_1 + a_2 + \sqrt{a_1 + a_2})$$

$$a_1 = 1 \text{ m} \times 1 \text{ m}$$

$$\begin{aligned} a_2 &= \frac{B}{2} \times \frac{B}{2} \\ &= \frac{11.25}{2} \times \frac{11.25}{2} = 31.64 \text{ m}^2 \end{aligned}$$

$$11.796 = \frac{h}{3} (1 + 31.64 + \sqrt{1 + 31.64})$$

$$h = \frac{11.796 \times 3}{38.265} = 0.925 \text{ m} \quad (h = 1 - 2)$$

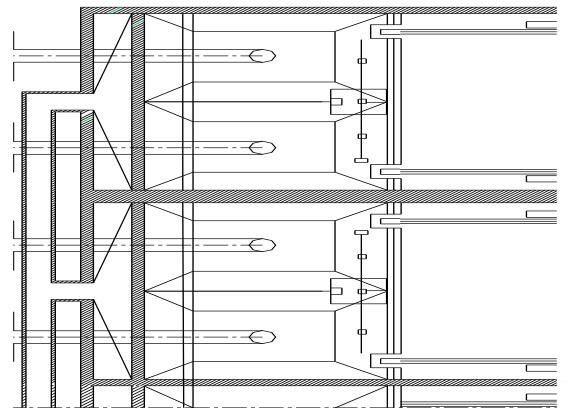
For circular tank:

$$V = \frac{\pi}{4} \left(\frac{\phi_b^2 + \phi_s^2}{2} \right) h$$

$$\phi_s \geq 1 \text{ m}$$

$$h = 1 - 2 \text{ m}$$

$$\theta = 45^\circ - 60^\circ$$



Design of sludge withdrawal pipe:

Assume time of withdrawal 5 minutes (5 – 20 minutes)

$$Q_{sludge} = \frac{11.796}{5 \times 60} = 0.039 \text{ m}^3 / \text{s}$$

$$Q_{sludge} = A \times v \quad v \text{ in sludge pipe} = 1 - 1.5 \text{ m/s}$$

$$0.039 = \frac{\pi \phi^2}{4} \times 1$$

$$\therefore \phi = 0.22 \text{ m} \approx 200 \text{ mm} \quad (\phi \geq 150 \text{ mm})$$

$$v_{act} = 1.24 \text{ m/s} \quad \text{safe}$$